

# **An Examination of the Oxygen Reduction Reaction on RuO<sub>2</sub>-based Oxide Coatings Formed on Titanium Substrates**

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## **Abstract**

The RuO<sub>2</sub>-based electrocatalysts were prepared by using a dip-coating method on Ti plate substrates at 400 °C. The catalytic activity of the oxide-coated electrodes for the oxygen reduction reaction (ORR) was evaluated by cyclic voltammetry in 0.5 M H<sub>2</sub>SO<sub>4</sub> at 60 °C in a stationary state. The examination was focused on the enhancement of the catalytic activity in the reaction by the enlargement of the surface area of the RuO<sub>2</sub> coating with the help of lanthanum. The onset potential for the ORR,  $E_{\text{ORR-0}}$ , of the RuO<sub>2</sub>/Ti electrode showed that the highest value was 0.84 V vs. RHE.

## **1. Introduction**

Platinum-based alloys are presently the typical cathode catalysts used for Polymer Electrolyte Fuel Cells (PEFCs) due to their high oxygen reduction activity. Since platinum is a highly expensive material, the development of catalysts to replace platinum, including oxides [1-3], carbides [4,5], and metal complexes [6,7], etc., has widely been examined by many research groups. Recently, some interesting studies on the development of Pt-free oxide cathodes, such as  $\text{TaO}_{0.92}\text{N}_{1.05}$  and  $\text{ZrO}_{2-x}$ , have been reported [8,9]. Although these and numerous other studies have significantly contributed to the development of PEFC and DMFC, further investigation is still required for the improvement of both activity and durability. The  $\text{RuO}_2\text{-TiO}_2/\text{Ti}$  binary and  $\text{IrO}_2\text{-RuO}_2\text{-TiO}_2/\text{Ti}$  ternary oxide electrodes are widely used as the Dimensionally Stable Anode (DSA<sup>®</sup>) catalyst-electrode in the electrolysis process for chlorine production in chlor-alkali industries [10]. Although basic investigations of the ORRs of ruthenium metal and compounds in acidic solutions have been published [11-14], few reports on crystalline ruthenium oxide in acidic solutions have been published [15].

This study presents a fundamental investigation of the development of non-Pt catalyst cathodes for PEFCs, using  $\text{RuO}_2$ -based oxides which were coated on a Ti plate substrate. This investigation using ruthenium oxide as the cathode is the first-step towards the development of less expensive and anti-corrosive oxide cathodes in the future.

## **2. Experiment**

### *2.1. Preparation of $\text{RuO}_2/\text{Ti}$ electrodes by a dip-coating method*

Rutile-type RuO<sub>2</sub> coating-film was prepared on a Ti plate (10×10×1 mm) substrate by a conventional dip-coating method using an ethylene glycol solution of ruthenium chloride ([RuCl<sub>3</sub>] = 0.5 M). The titanium substrates were etched with 10% oxalic acid at 80 °C for 1 h, and then rinsed with deionized water before the dipping procedure. Calcination of the dip-coated salts was conducted in air at 400 °C. The dip-drying/calcination (alternating 10 min each) procedure was repeated 10 times. RuO<sub>2</sub>/Ti electrodes with extremely enlarged surface areas were prepared using a dip-coating solution containing RuCl<sub>3</sub> and LaCl<sub>3</sub> in ethylene glycol ([RuCl<sub>3</sub>] = [LaCl<sub>3</sub>] = 0.5 M) [16, 17]. After the dip-drying/calcination (400 °C, 10 min) procedure was repeated 10 times, any of the lanthanum species were removed with 0.5 M H<sub>2</sub>SO<sub>4</sub> at 80 °C. According to the Energy Dispersive X-ray Fluorescence Spectroscopy (EDX) analysis, the complete removal of the La<sub>2</sub>O<sub>3</sub> by the acid treatment was confirmed. This electrode was denoted as the La<sub>2</sub>O<sub>3</sub>-treated RuO<sub>2</sub>/Ti electrode in this study.

Individual oxides: RuO<sub>2</sub> and binary oxides of RuO<sub>2</sub> mixed with either MoO<sub>x</sub> and VO<sub>x</sub> were also prepared on Ti substrates by a dip-coating method using ethylene glycol solutions of metal salts: RuCl<sub>3</sub>, MoCl<sub>5</sub> and VOCl<sub>3</sub>. Calcination of the dip-coated salts was conducted at 400 °C in air. The dipping-drying-calcination procedure was repeated 10 times in order to prepare electrodes that showed reproducible performance. These oxide electrodes are denoted as the RuO<sub>2</sub>/Ti, RuMo(1:1)O<sub>x</sub>/Ti and RuV(1:1)O<sub>x</sub>/Ti electrodes.

## 2.2. Electrochemical measurements

The ORR activity of the oxide electrodes was evaluated by cyclic voltammetry (CV) in 0.5 M H<sub>2</sub>SO<sub>4</sub> using a beaker-type electrolytic cell (Fig. 1), in a stationary state at 60 °C.

A carbon felt, rather than Pt, was used as the counter electrode in order to avoid the deposition of Pt onto the test electrode through dissolution. Although an Ag/AgCl reference electrode was used, the electrode potential is presented vs RHE. A Luggin capillary faced the working electrode at a distance of 2 mm. All electrode potentials are referred to the RHE(*t*) scale, corrected for temperature effect. For the ORR experiment, oxygen gas was bubbled into the 0.5 M H<sub>2</sub>SO<sub>4</sub> solution at 60 °C.

### **3. Results and discussion**

#### *3.1 ORR activity of RuO<sub>2</sub>/Ti electrodes enhanced by the morphological modification of the oxide layers*

Figure 2-(a) shows CVs of the RuO<sub>2</sub>/Ti electrode in N<sub>2</sub>-saturated 0.5 M H<sub>2</sub>SO<sub>4</sub> (dotted line) and in O<sub>2</sub>-saturated 0.5 M H<sub>2</sub>SO<sub>4</sub> (solid line). During both potential scans (anodic and cathodic potential sweeps), an additional cathodic current was observed for the CV measured with an O<sub>2</sub>-saturated solution, as compared with the measured with an N<sub>2</sub>-saturated solution. This additional cathodic current is due to the ORR on the oxide electrode. In order to enhance the ORR activity of this oxide electrode, we have tried to use lanthanum to enlarge the surface area of the oxide [16,17]. When a DSA-type binary oxide electrode was prepared with a dip-coating solution containing ruthenium salt and a rare earth salt, the resulting electrode was composed of a composite oxide of each element so long as the calcination temperature was not too high. Since the rare earth oxide can easily be removed by acid, a porous RuO<sub>2</sub> layer with an extremely enlarged surface area remained after the acid treatment of the composite electrode. Figure 2-(b) shows CVs of the La<sub>2</sub>O<sub>3</sub>-treated

RuO<sub>2</sub>(Ru:La=1:1)/Ti electrode in N<sub>2</sub>-saturated 0.5 M H<sub>2</sub>SO<sub>4</sub> (dotted line) and in O<sub>2</sub>-saturated 0.5 M H<sub>2</sub>SO<sub>4</sub> (solid line). Obviously, the pseudocapacitance of the La<sub>2</sub>O<sub>3</sub>-treated RuO<sub>2</sub>(Ru:La=1:1)/Ti electrode, (b), is much higher than that of the RuO<sub>2</sub>/Ti electrode, (a). To clarify the enhancement effect of the La<sub>2</sub>O<sub>3</sub>-treatment, the molar ratio of La to Ru in the dip-coating solution was changed, and the ORR behaviors of those electrodes were evaluated. Figure 3 shows the ORR cathodic current curves for the electrodes presented in each geometric surface area, which were obtained by subtracting the voltammogram of the O<sub>2</sub>-saturated solution during a cathodic scan from that of the N<sub>2</sub>-saturated electrolytes. Since the voltammetry was carried out under a stationary state, the ORR current densities of these electrodes must be compared carefully. However, it can be said that the cathodic current and the  $E_{\text{ORR}-0}$  for the ORR increases with an increase in the molar ratio of La to Ru. The onset electrode potential,  $E_{\text{ORR}-0}$ , for the ORR is defined by the potential where the additional cathodic current begins to be observed on the voltammogram, and that of  $E_{\text{ORR}-20}$  is the potential where the additional cathodic current attained to 20  $\mu\text{A}/\text{cm}^2$ -(geometric). The onset electrode potentials for the ORR on RuO<sub>2</sub>/Ti, RuO<sub>2</sub>(Ru:La=9:1)/Ti, RuO<sub>2</sub>(Ru:La=7:3)/Ti and RuO<sub>2</sub>(Ru:La=1:1)/Ti are listed in Table 1. Among these electrodes, the RuLa(1:1)O<sub>2</sub>/Ti electrode showed the highest activity for the ORR.

The La<sub>2</sub>O<sub>3</sub>-treated RuO<sub>2</sub>/Ti electrodes which were prepared with much more lanthanum content than 1:1 were unstable after the dissolution of La<sub>2</sub>O<sub>3</sub> from the RuO<sub>2</sub>-La<sub>2</sub>O<sub>3</sub> composite oxide layers in acid. The RuO<sub>2</sub>/Ti electrode, (a), prepared by this dip-coating method showed typical surface morphology as shown in Fig. 4-(a). As shown in the four High Resolution Scanning Electron Microscopy (HRSEM) images in Fig. 4, the size of the RuO<sub>2</sub> particles decreased

with an increase in the molar ratio of La to Ru. Qualitatively, it could be said that the reason that the increase in the catalytic activity of the RuO<sub>2</sub>/Ti electrode for the ORR increases with the La to Ru ratio is accounted for by the increase of the surface area of the porous RuO<sub>2</sub> layers. As shown in the X-ray diffraction (XRD) patterns of the RuO<sub>2</sub>/Ti and the RuO<sub>2</sub>(Ru:La=1:1)/Ti electrodes shown in Fig. 5, rutile-type RuO<sub>2</sub> was formed on the Ti substrate under the preparation conditions. The difference of the particle size of RuO<sub>2</sub> shown in Fig. 4 reflects both on the peak intensity and the half width of the diffraction patterns of these electrodes. Thus, the crystallite size of the RuO<sub>2</sub> of the latter electrode is also smaller than that of the former electrode. Although the XRD pattern of the latter electrode was taken after the dissolution of lanthanum species in the oxide layer by acid, an unknown peak was observed around  $2\theta = 43.8^\circ$ . The possibility of the formation of a small amount of a ruthenium compound with lanthanum can not be excluded, while lanthanum was not detected by the EDX.

### *3.2 ORR activity of RuO<sub>2</sub>/Ti electrodes enhanced by the addition of other elements*

Since both IrMoO<sub>2</sub>/Ti and IrVO<sub>2</sub>/Ti showed a high activity for the ORR as reported in the previous paper [18], the effect of the addition of either molybdenum or vanadium to RuO<sub>2</sub> was examined. For the binary electrodes, RuMo(1:1)O<sub>2</sub>/Ti and RuV(7:3)O<sub>2</sub>/Ti, most of the molybdenum and vanadium remained in each of the oxide layers even after the HCl treatment at 80 °C. As shown in Fig. 6, the enhancement effect of the addition of these elements to RuO<sub>2</sub> was not so great, so long as the content ratios. In the previous paper concerning the enhancement of the ORR activity of the IrO<sub>2</sub>/Ti electrode, we confirmed that the following two methods are effective for the oxide catalyst

electrode: the first method is the formation of a solid solution to change the valency of iridium ions with another element [18], and the second method is the use of rare earth elements to enlarge the surface area of oxides [16,17]. However, the first effect was moderate for the RuO<sub>2</sub>-based electrode in comparison with the IrO<sub>2</sub>-based electrode. Figure 7 compares the polarization curves for the ORR of RuO<sub>2</sub>-based electrodes with those of IrO<sub>2</sub>-based and a platinum plate electrodes, and Table 2 presents the  $E_{\text{ORR}}$  values of these electrodes including the RuMo(1:1)O<sub>2</sub>/Ti and RuV(7:3)O<sub>2</sub>/Ti. As has been discussed in the previous paper [18], the porous Ir<sub>0.6</sub>V<sub>0.4</sub>O<sub>2</sub>/Ti electrode showed the onset potentials for the ORR to be  $E_{\text{ORR}} = 0.90$  V and  $E_{\text{ORR-20}} = 0.86$  V vs RHE and exhibited higher activity than that of a flat Pt plate electrode at 0.8 V (vs RHE), when the current density for the ORR was evaluated with the geometric surface area. This oxide electrode may have a roughness factor of several decades; therefore, the actual effective surface area of this porous oxide electrocatalyst requires evaluation. The catalytic activity for the ORR of the RuO<sub>2</sub>-based electrodes is lower than those of IrO<sub>2</sub>-based electrodes; however, it is noteworthy that the catalytic activity of RuO<sub>2</sub>/Ti electrode for the ORR can be greatly enhanced by the formation of fine RuO<sub>2</sub> particles connecting to each other on the titanium substrate.

## Conclusions

As has been discussed in the previous paper [18,19], the porous Ir<sub>0.6</sub>V<sub>0.4</sub>O<sub>2</sub>/Ti electrode exhibited twice the activity of a flat Pt plate electrode at 0.8 V (vs RHE), when the current density for the ORR was evaluated for the geometric surface area. Although the ORR activity of the La<sub>2</sub>O<sub>3</sub>-treated RuO<sub>2</sub>/Ti was still

lower than the platinum electrode, the enlargement of the surface area of the RuO<sub>2</sub>/Ti oxide electrode with the help of lanthanum can considerably enhance the catalytic activity of the RuO<sub>2</sub>/Ti oxide electrode. This modification method of the morphology of the oxide layer must provide useful information on the design of the oxide cathode catalysts using less-expensive elements.

DSA-type electrodes have many advantages: the coating layer is composed of fine oxide particles connected to each other to form a micro/meso porous structure, the titanium substrate is protected from corrosion by the formation of a dense oxide layer at the interface between the porous oxide coating and titanium substrate, and preparation of the electrodes is easy and useful for the search of new electrocatalysts.

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### Figure captions

Fig. 1 The electrochemical cell and setup

Fig.2 Cyclic voltammograms of the RuO<sub>2</sub>/Ti and RuO<sub>2</sub>(Ru:La=1:1)/Ti electrodes.

Electrodes: (a) RuO<sub>2</sub>/Ti and (b) RuO<sub>2</sub>(Ru:La=1:1)/Ti.

The broken lines indicate measurement in N<sub>2</sub>-saturated electrolyte and the solid lines indicate O<sub>2</sub>-saturated electrolyte. The current density is presented as current per geometric surface area of the electrodes.

Electrolyte: 0.5 M H<sub>2</sub>SO<sub>4</sub> (60 °C). Sweep rate: 5 mV s<sup>-1</sup>.

Fig. 3 The ORR-current curves of various RuO<sub>2</sub>-based electrodes.

Electrodes: (a) RuO<sub>2</sub>/Ti, (b) RuO<sub>2</sub>(Ru:La=9:1)/Ti, (c) RuO<sub>2</sub>(Ru:La=7:3)/Ti and (d) RuO<sub>2</sub>(Ru:La=1:1)/Ti. Electrolyte: 0.5 M H<sub>2</sub>SO<sub>4</sub> (60 °C). Sweep rate: 5 mV s<sup>-1</sup>.

Fig. 4 High magnification SEM images of the RuO<sub>2</sub>-based electrodes.

Electrodes: (a) RuO<sub>2</sub>/Ti, (b) RuO<sub>2</sub>(Ru:La=9:1)/Ti, (c) RuO<sub>2</sub>(Ru:La=7:3)/Ti and

(d)  $\text{RuO}_2(\text{Ru}:\text{La}=1:1)/\text{Ti}$ .

Fig. 5 XRD patterns of the  $\text{RuO}_2/\text{Ti}$  and  $\text{RuO}_2(\text{Ru}:\text{La}=1:1)/\text{Ti}$  electrodes.

Electrodes: (a)  $\text{RuO}_2/\text{Ti}$  and (b)  $\text{RuO}_2(\text{Ru}:\text{La}=1:1)/\text{Ti}$

Lanthanum species was removed by 0.5 M  $\text{H}_2\text{SO}_4$  at 80 °C. So long as the EDX analysis, the complete removal of the  $\text{La}_2\text{O}_3$  by the acid treatment was confirmed.

Fig. 6 The ORR-current curves of various  $\text{RuO}_2$ -based electrodes.

Electrodes: (a)  $\text{RuO}_2/\text{Ti}$ , (b)  $\text{RuMo}(1:1)\text{O}_2/\text{Ti}$ , (c)  $\text{RuV}(1:1)\text{O}_2/\text{Ti}$  and (d)  $\text{RuO}_2(\text{Ru}:\text{La}=1:1)/\text{Ti}$ . Electrolyte: 0.5 M  $\text{H}_2\text{SO}_4$  (60 °C). Sweep rate: 5  $\text{mV s}^{-1}$ .

Fig. 7 The ORR-current curves of various  $\text{RuO}_2$ - and  $\text{IrO}_2$ -based electrodes.

Electrodes: (a)  $\text{RuO}_2/\text{Ti}$ , (b)  $\text{IrO}_2/\text{Ti}$ , (c)  $\text{RuO}_2(\text{Ru}:\text{La}=1:1)/\text{Ti}$  and (d)  $\text{IrV}(1:1)\text{O}_2/\text{Ti}$ , (e) a Pt plate. Electrolyte: 0.5 M  $\text{H}_2\text{SO}_4$  (60 °C). Sweep rate: 5  $\text{mV s}^{-1}$ .

Table 1 The onset electrode potentials for the ORR on RuO<sub>2</sub>-based electrodes.

Potential V (vs RHE)	RuO <sub>2</sub> /Ti	RuO <sub>2</sub> (Ru:La=9:1)O <sub>x</sub> /Ti	RuO <sub>2</sub> (Ru:La=7:3)O <sub>x</sub> /Ti	RuO <sub>2</sub> (Ru:La=1:1)O <sub>x</sub> /Ti
$E_{\text{ORR-0}}$	0.73	0.70	0.77	0.83
$E_{\text{ORR-20}}$	0.50	0.65	0.70	0.79

The definition of  $E_{\text{ORR-0}}$  and  $E_{\text{ORR-20}}$  is described in the text.

Table 2 The onset electrode potentials for the ORR on RuO<sub>2</sub>- and IrO<sub>2</sub>-based oxide electrodes.

Potential V (vs RHE)	RuMo(1:1)O <sub>2</sub> /Ti	RuV(7:3)O <sub>x</sub> /Ti	RuV(1:1)O <sub>x</sub> /Ti	IrO <sub>2</sub> /Ti	IrMo(1:1)O <sub>2</sub> /Ti	IrV(1:1)O <sub>2</sub> /Ti <sup>a)</sup>	Pt
$E_{\text{ORR-0}}$	0.70	0.65	0.70	0.84	0.87	0.90	0.89
$E_{\text{ORR-20}}$	0.58	0.55	0.58	0.74	0.79	0.86	0.82

The definition of  $E_{\text{ORR-0}}$  and  $E_{\text{ORR-20}}$  is described in the text. a) After the acid-treatment, the IrV(1:1)O<sub>2</sub>/Ti electrode changed into Ir<sub>0.6</sub>V<sub>0.4</sub>O<sub>2</sub>/Ti due to the partial dissolution of vanadium species.

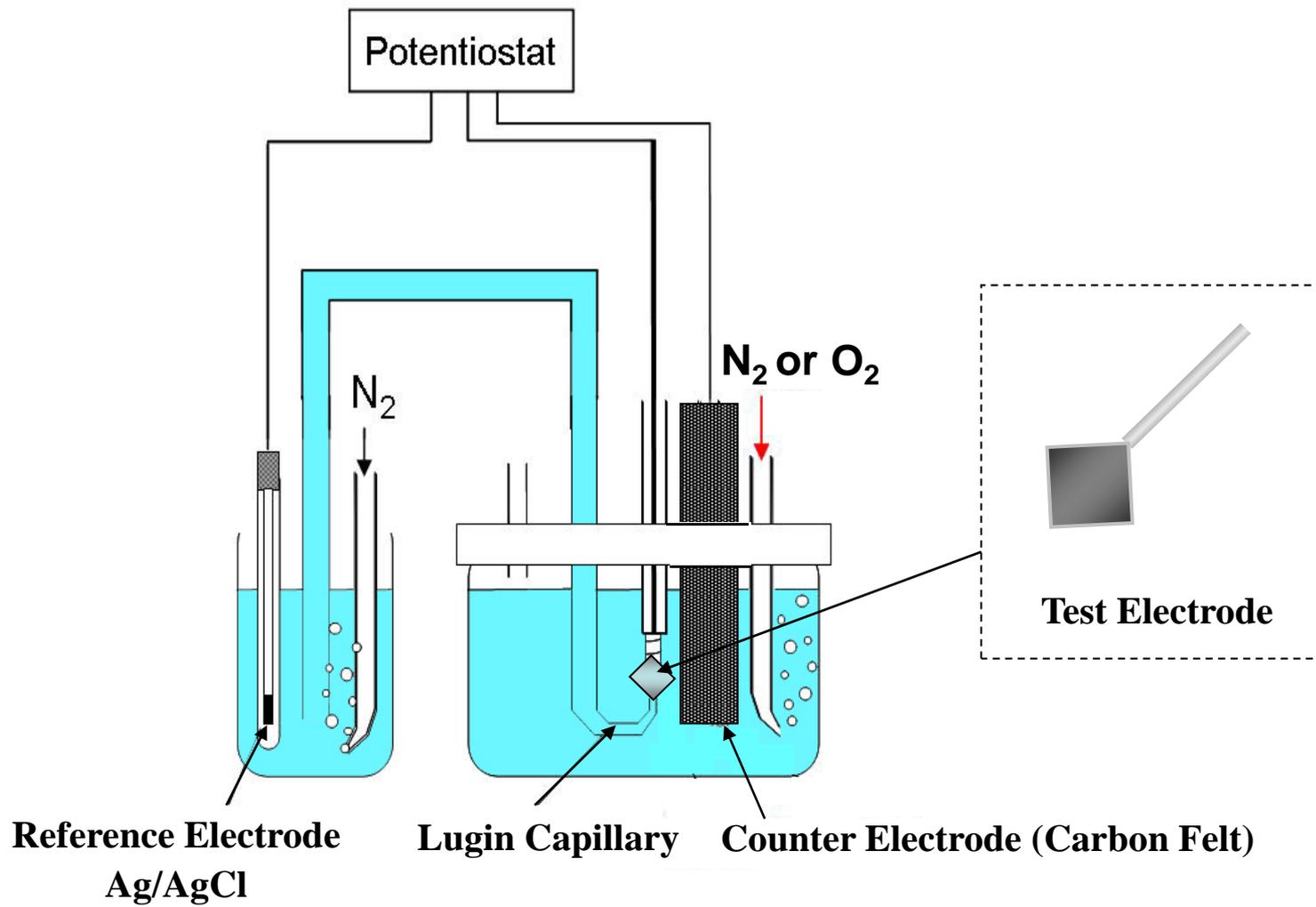


Fig. 1 Y.Takasu et al.

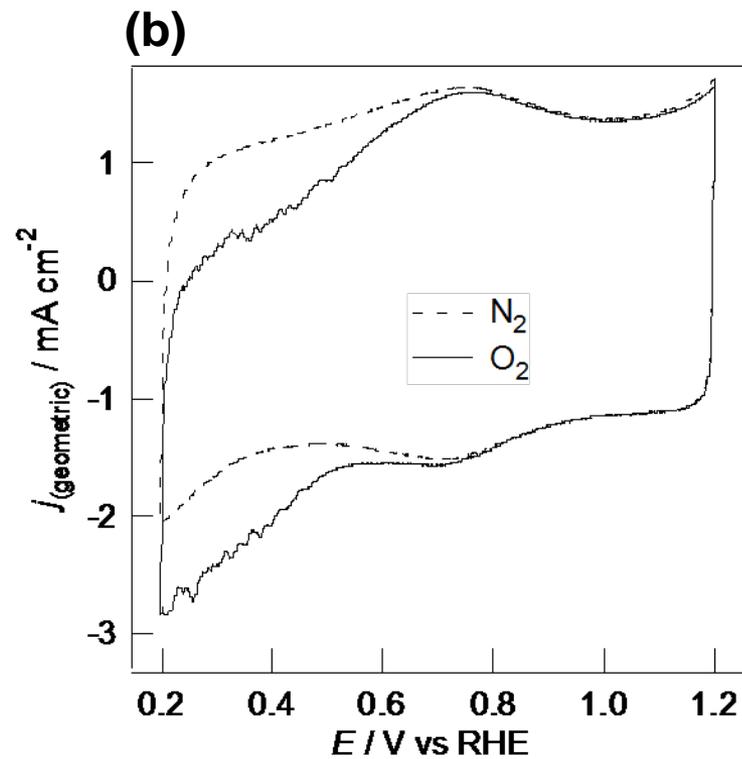
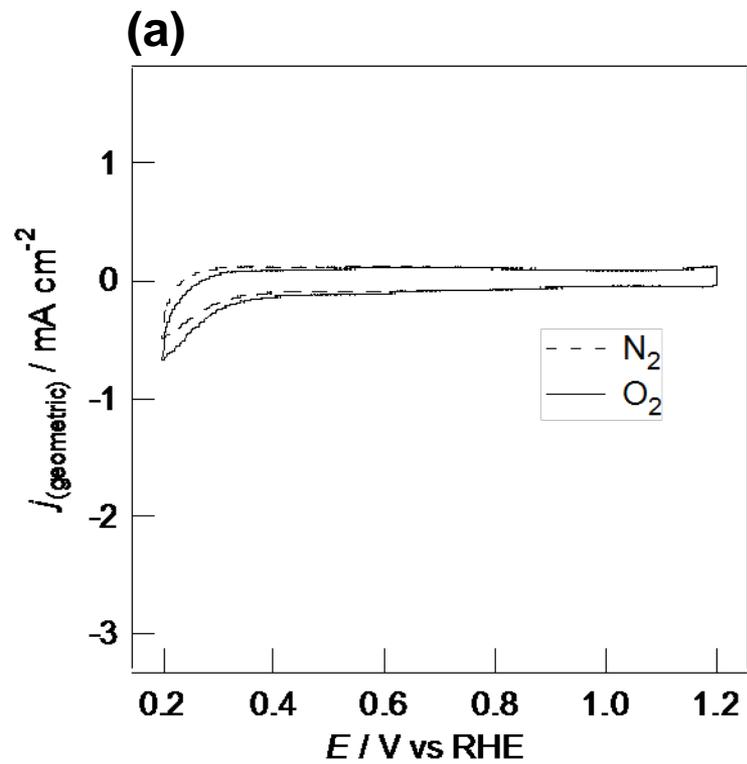
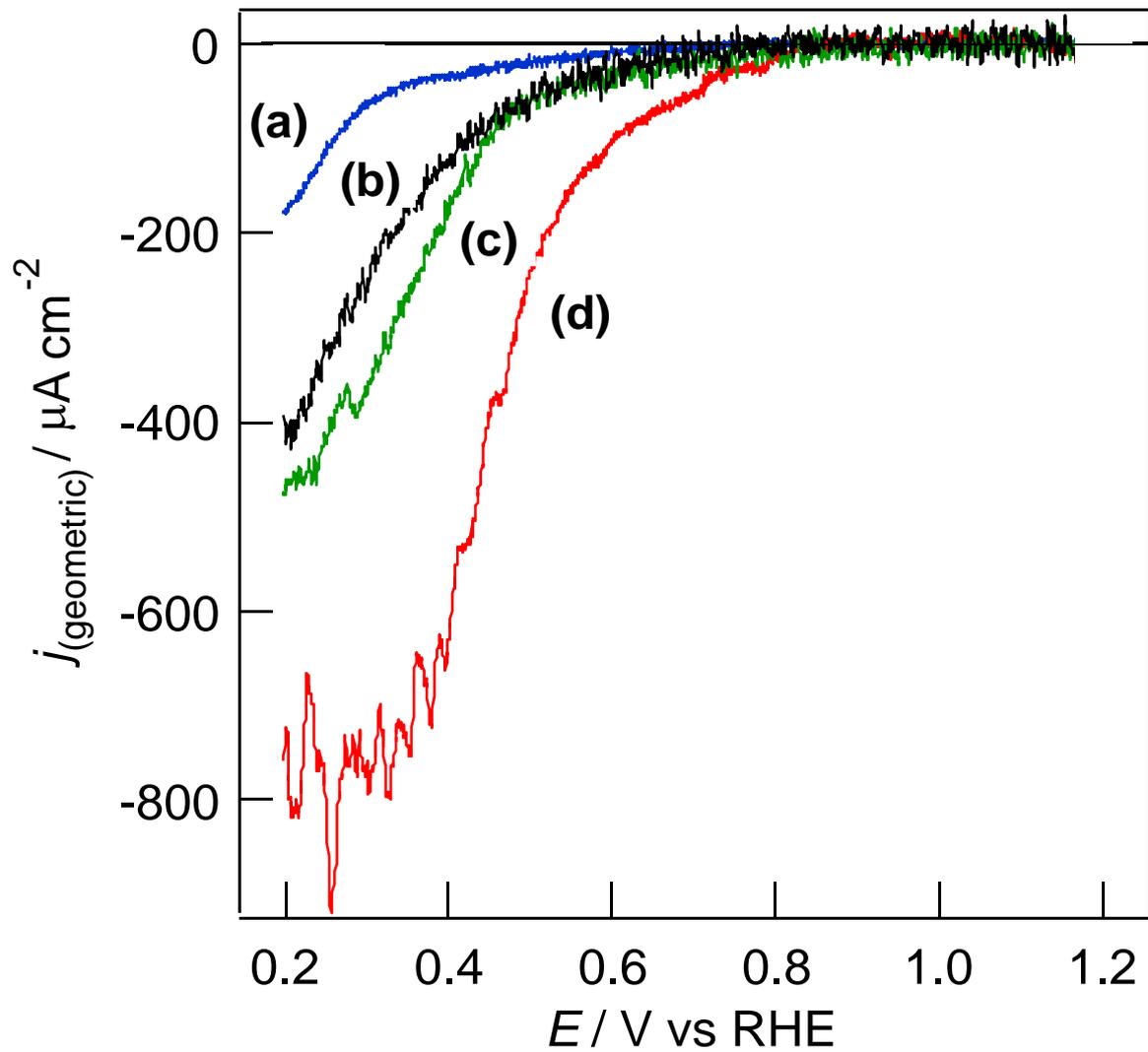
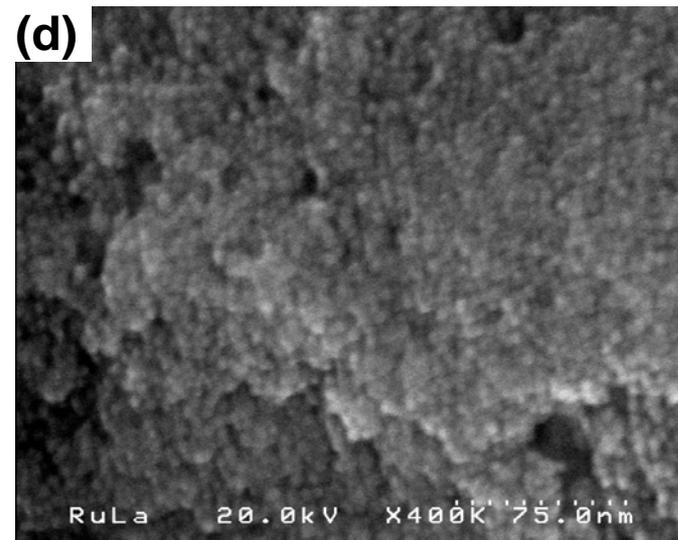
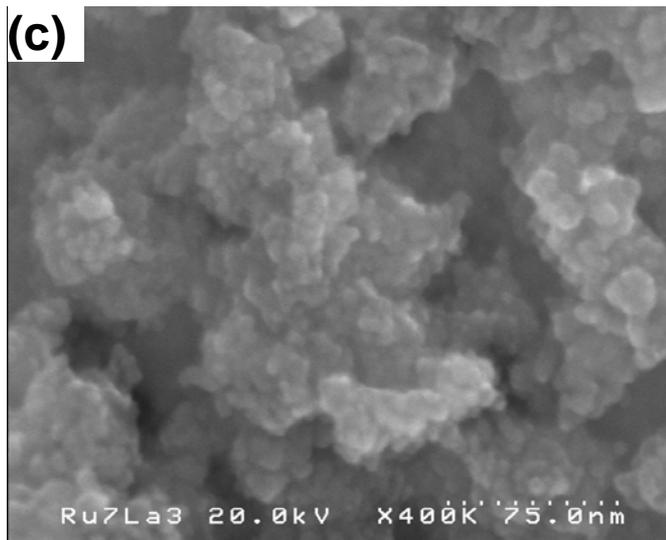
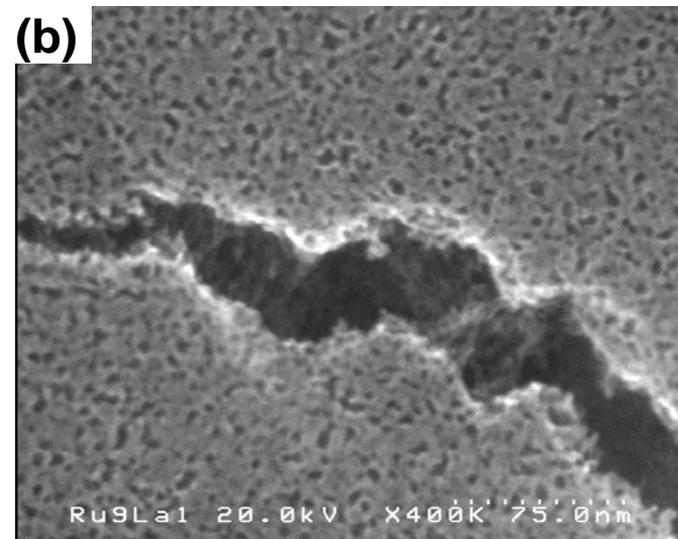
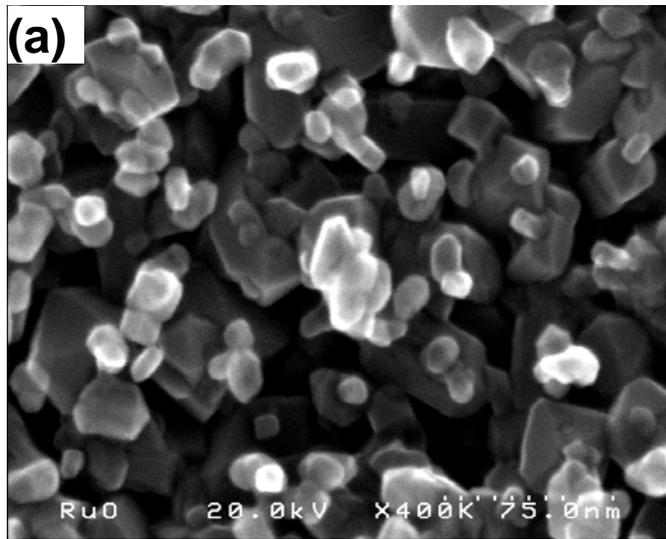


Fig. 2 Y.Takasu et al.



**Fig. 3** Y.Takasu et al.



**Fig. 4** Y.Takasu et al.

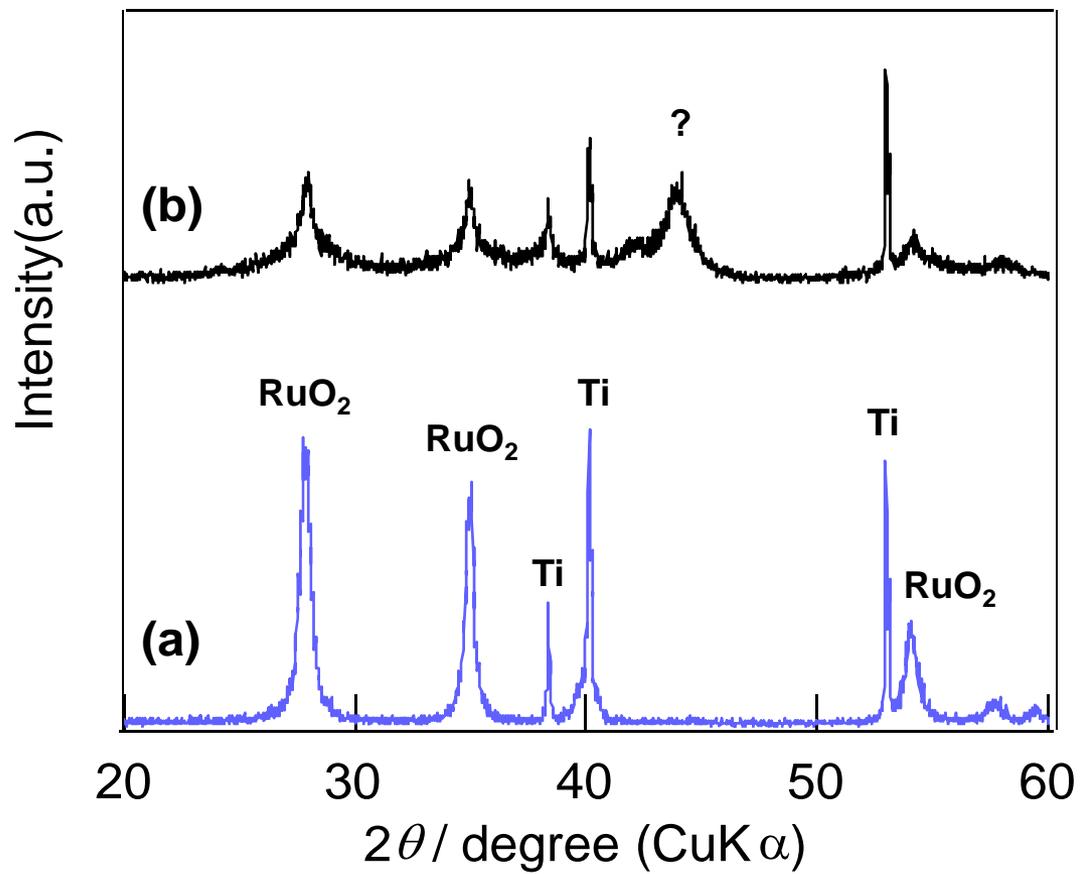


Fig. 5 Y.Takasu et al.

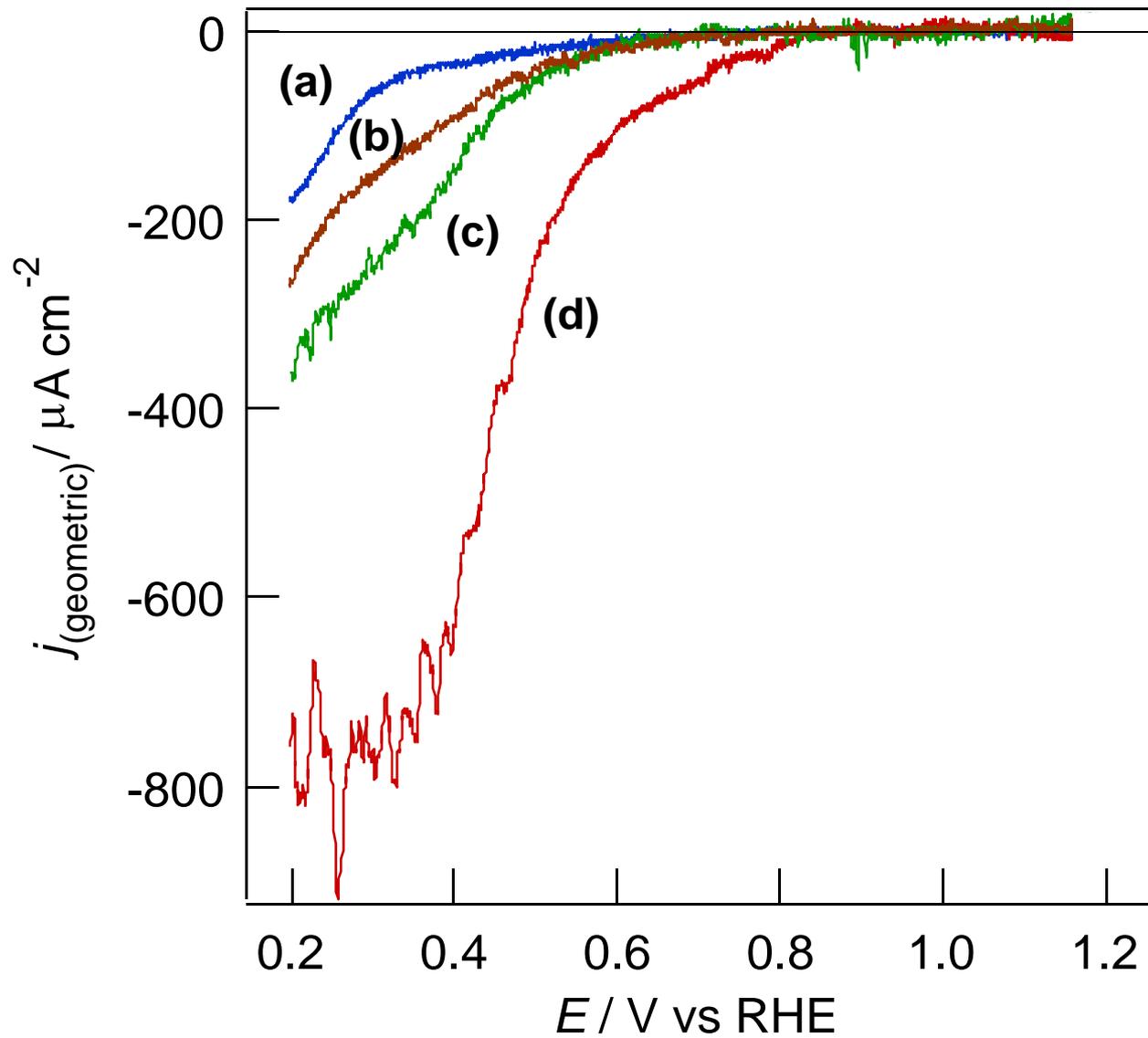


Fig. 6 Y.Takasu et al.

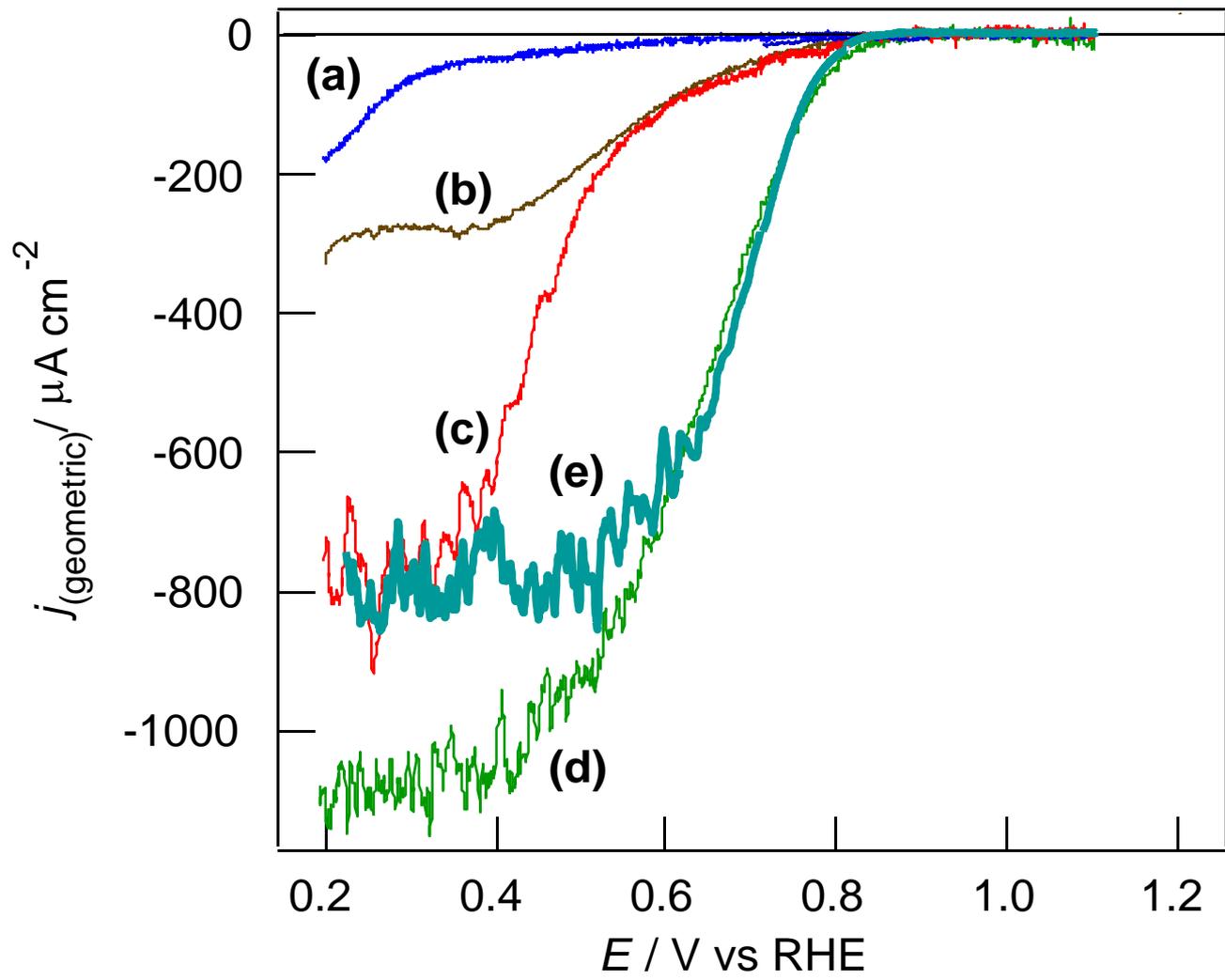


Fig. 7 Y.Takasu et al.